



## Interconnected-Tubes Model of Hepatic Elimination: Steady-state Considerations

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In the interconnected-tubes model of hepatic transport and elimination, intermixing between sinusoids was modelled by the continuous interchange of solutes between a set of parallel tubes. In the case of strongly interconnected tubes and for bolus input of solute, a zeroth-order approximation led to the governing equation of the dispersion model. The dispersion number was expressed for the first time in terms of its main physiological determinants: heterogeneity of flow and density of interconnections. The interconnected-tubes model is now applied to steady-state hepatic extraction. In the limit of strong interconnections, the expression for output concentrations is predicted to be similar in form to those predicted by the distributed model for a narrow distribution of elimination rates over sinusoids, and by the dispersion model in the limit of a small dispersion number  $D_N$ . More generally, the equations for the predicted output concentrations can be expressed in terms of a dimensionless 'heterogeneity number'  $H_N$ , which characterizes the combined effects of variations in enzyme distribution and flow rates between different sinusoids, together with the effects of interconnections between sinusoids. A comparative analysis of the equations for the dispersion and heterogeneity numbers shows that the value of  $H_N$  can be less than, greater than or equal to the value of  $D_N$  for a correlation between distributions of velocities and elimination rates over sinusoids, anticorrelation between them, and when all sinusoids have the same elimination rate, respectively. Simple model systems are used to illustrate the determinants of  $H_N$  and  $D_N$ .

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### 1. Introduction

The prediction of hepatic extraction in terms of changes in hepatic blood flow, solute binding in the blood and hepatic enzyme activity is of clinical importance. The well-stirred model has been widely used as illustrated in the recent work on the prediction of hepatic extraction under vary

ing conditions of cardiac output (Schoemaker *et al.*, 1998); the dispersion model has also been widely applied, especially in the prediction of human hepatic extraction of solutes from their *in vitro* metabolic clearances in human hepatocytes or microsomes (Iwatsubo *et al.*, 1997); and the distributed model has been used to predict various aspects of steady-state extraction (Bass, 1980; Bass & Keiding, 1988).

Whilst the well-stirred model represents the liver as one completely mixed compartment or tank, the dispersion model represents it as

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a “chemical reactor”, and aims to take account of (1) the variations in the flow velocity and in the lengths of different sinusoids, (2) mixing of blood at the branch points of sinusoids and at the interconnections between sinusoids, and (3) in principle, molecular diffusion, in terms of a “dispersion number”  $D_N$ , average flow-velocity  $v_{av}$ , and average elimination rate  $k_{av}$  appearing in a partial differential equation of convection–diffusion–reaction form. A limitation of the dispersion model has been the limited understanding and mathematical description of its defining stochastic parameter, the dispersion number  $D_N$ . To date, almost all studies exploring the determinants and magnitude of  $D_N$  have been experimental, measuring outflow concentrations after injection into the liver. Such studies have included bolus inputs of vascular references (Roberts & Rowland, 1986a), steady-state extraction (Roberts & Rowland, 1986b), metabolite formation (Roberts & Rowland, 1986c) and microsomal enzyme clearances (Roberts & Rowland, 1986d). Bass *et al.* (1987) and Roberts *et al.* (1988) recognized that the dispersion number was determined by vascular dispersion and enzyme distribution along the liver sinusoids. Vascular dispersion, which can be determined by the outflow concentration–time profile of a vascular reference, has been shown to be relatively independent of hepatic flow rate and blood composition (Roberts *et al.*, 1990a), coadministration of vasoactive substances (Roberts *et al.*, 1990b), age and species differences (Roberts *et al.*, 1999), hepatic regeneration after partial hepatectomy (Weiss *et al.*, 1998) and ischaemia reperfusion (unpublished data). Whilst enzyme heterogeneity (Bass *et al.*, 1987; Roberts *et al.*, 1988), axial diffusion (Rivory *et al.*, 1992) and radial tissue diffusion (Luxon & Weisiger, 1993; Weiss & Roberts, 1996) affect interpretation of the dispersion number, most recent experimental studies have found that the dispersion number for extracted solutes,  $D_N^E$ , is similar to that for vascular dispersion,  $D_N^V$ , for bolus input experiments (Chou *et al.*, 1993; Hussein *et al.*, 1994; Evans *et al.*, 1983; Hung *et al.*, 1998a, b). The exception in this analysis appears to be the dependence of taurocholate hepatic extraction on its fraction unbound in perfusate, presumably due to Bass-Pond effects (i.e. limitation in dis-

sociation from proteins and diffusion to anion pumps) (Roberts *et al.*, 1990a).

The distributed model (Bass *et al.*, 1978; Bracken & Bass, 1979) represents the sinusoids of the liver as a very large ensemble of  $n$  functionally independent tubules over which there is a distribution of blood flow rates  $f_j$  and enzymatic elimination rates  $k_{ej}$ , for  $j = 1, 2, \dots, n$ . (We consider only the limit of linear kinetics.) Assumptions are not needed in the model regarding either the constancy of cross-sectional areas of sinusoids, or their lengths, but for the present purposes it is convenient to simplify the modelling and suppose that each sinusoid has a constant area of cross-section, say  $a_j$  for the  $j$ th one, and that all the sinusoids have the same length  $L$ . The velocity of blood flow through the  $j$ th sinusoid is constant under the first of these further assumptions, at the value  $v_j = f_j/a_j$ . In terms of these modified assumptions and variables, and in the case that the distribution of elimination rates is narrow, the model enables steady-state hepatic extraction to be expressed in the form (Bass, 1980)

$$E = 1 - \exp(-R_N(1 + \frac{1}{2}\varepsilon^2 R_N^2)), \quad (1)$$

with  $\varepsilon^2 \ll 1$ . Here  $R_N$  is the dimensionless “efficiency number” (Roberts & Rowland, 1986a) given by

$$R_N = \frac{k_{av}V}{F} = \frac{k_{av}L}{v_{av}}, \quad (2)$$

and the dimensionless parameter  $\varepsilon^2$  is given by

$$\varepsilon^2 = \frac{1}{F} \sum_{j=1}^n f_j \left( \frac{k_{ej}/k_{av}}{v_j/v_{av}} \right)^2 - 1. \quad (3)$$

In eqn (2) and (3),  $V = AL$  is the total liver (sinusoidal) volume,  $F = \sum_{j=1}^n f_j$  is the total blood flow rate through the liver,  $A = \sum_{i=1}^n a_i$  is the total area of cross-section of sinusoids, and  $v_{av}$ ,  $k_{av}$  are average sinusoidal velocity and elimination rate, respectively, defined as

$$v_{av} = \frac{F}{A}, \quad k_{av} = \frac{1}{A} \sum_{i=1}^n a_i k_{ei}. \quad (4)$$

Roberts & Rowland (1985, 1986a) have shown that different forms of the dispersion model yield an equation similar in form to eqn (1), when  $D_N \ll 1$  and a uniform enzyme distribution along sinusoids is assumed

$$E = 1 - \exp(-R_N(1 + D_N R_N^2)). \quad (5)$$

In their study of the relationship between eqns (1) and (5), Bass *et al.* (1987) recognized that  $D_N$  used in equation (5), which we will refer to as  $D_N^E$  for clarity to represent the dispersion number defined by hepatic extraction, has two components, one due to heterogeneity of enzyme distribution in sinusoids, and the other due to vascular dispersion. They limited their considerations of enzyme heterogeneity to longitudinal distribution of enzymes. Roberts *et al.* (1988) recognized that transverse enzyme distribution was also important but limited their analysis to numerical simulations. Comparing the distributed model with the dispersion model for  $D_N^E \ll 1$ , Bass *et al.* (1987) suggested that the dispersion number for extracted solutes under the condition of steady-state input can be expressed explicitly as

$$D_N^E = D_N^a \frac{\overline{\rho^2}}{\bar{\rho}^2} = \frac{1}{2} \varepsilon^2. \quad (6)$$

Here  $D_N^a$  is the *apparent* dispersion number, defined predominantly by the vascular dispersion (as can be obtained from the outflow profile of a non-extracted vascular reference after bolus administration), but also by the transverse enzyme heterogeneity. Also in eqn (6),  $\rho(x)$  is a density function which describes distribution of enzyme along liver sinusoids (assumed by Bass *et al.* to be the same for all sinusoids), and

$$\bar{\rho} = \frac{1}{L} \int_0^L \rho(x) dx, \quad \overline{\rho^2} = \frac{1}{L} \int_0^L \rho(x)^2 dx. \quad (7)$$

The interconnected-tubes model of hepatic elimination was developed, in part to provide a firmer physiological basis for the dispersion model, and to identify better the underlying determinants of the dispersion number in a mathematically precise and rigorous manner. Our initial analysis was limited to the construc-

tion of the model and its application to the specific case of the outflow concentration–time profile following bolus input (Anissimov *et al.*, 1997). It was shown that the zeroth-order approximation of the interconnected-tubes model is equivalent in form to the dispersion model and that the dispersion number can be explicitly expressed in terms of the determinants (1) heterogeneity of flow and (2) density of interconnections between sinusoids. It is important to note that the dispersion number as derived in this approximation does not involve heterogeneity of the elimination rates. The simplest form of the model, in comparison with experimental data, yielded an estimate of about ten interconnections, on average, between sinusoids.

We now consider the application of the interconnected-tubes model to the case of steady-state hepatic extraction. A specific goal is to clarify further the effects of enzyme heterogeneity and vascular dispersion on the dispersion number, complementing the study of Bass *et al.* (1987) and Roberts *et al.* (1988), and to do this in a more exact form using the mathematical analysis of the interconnected-tubes model. We shall show that the steady-state extraction of solutes is defined by a heterogeneity number as well as the efficiency number common to the various hepatic elimination models (Roberts & Rowland, 1986a). This heterogeneity number depends on both micro-mixing and transverse enzyme heterogeneity.

## 2. Brief Review: Interconnected-Tubes Model and Bolus Input

In order to describe both the sinusoidal structure of the liver, and the high degree of intermixing observed experimentally (Koo *et al.*, 1975), we modelled the elimination process in terms of a large number  $n$  of tubes acting in parallel, with various flow rates, with elimination within each tube, and with continuous interchange of substrate between tubes along their (common) length  $L$  (Anissimov *et al.*, 1997). For linear elimination kinetics, and under simplifying assumptions that cross-sectional areas, flow rates, elimination rate constants and coefficients describing exchange of solute between tubes are all constant along the tubes, the governing equations of the

interconnected-tubes model in matrix form are (Anissimov *et al.*, 1997)

$$\frac{\partial \mathbf{c}(x, t)}{\partial t} = -\mathbf{V} \frac{\partial \mathbf{c}(x, t)}{\partial x} - \mathbf{K}_e \mathbf{c}(x, t) + \mathbf{M} \mathbf{c}(x, t), \quad (8)$$

where  $t$  is the time,  $x$  the distance along the tubes from input at  $x = 0$  to output at  $x = L$ ,  $\mathbf{c}(x, t) = (c_1(x, t), c_2(x, t), \dots, c_n(x, t))^T$  and  $\mathbf{V} = \text{diag}(v_i)$ ,  $\mathbf{K}_e = \text{diag}(k_{ei})$  and  $\mathbf{M}$  are  $n \times n$  matrices. For the  $i$ -th tube,  $c_i(x, t)$  is the concentration,  $v_i$  is the (constant) velocity of blood flow,  $k_{ei}$  is the elimination rate constant and  $a_i$  is the (constant) cross-sectional area. In addition,  $\mathbf{M} = \{m_{ij}\}$  is the matrix of coefficients of exchange between tubes, so that

$$m_{ij} = -\delta_{ij} \sum_{l=1}^n k_{il} + k_{ji} \frac{a_j}{a_i}, \quad i, j = 1, \dots, n, \quad (9)$$

where  $k_{ij}$  is the constant coefficient of exchange from tube  $i$  to tube  $j$ . Due to physical constraints and consistency conditions on the system of interconnected tubes, the matrix  $\mathbf{M}$  has the properties (Anissimov *et al.*, 1997)

$$\mathbf{a}^T \mathbf{M} = 0, \quad \mathbf{M} \mathbf{e} = 0, \quad \text{rank}(\mathbf{M}) = n - 1, \quad (10)$$

where  $\mathbf{a} = (a_1, a_2, \dots, a_n)^T$  and  $\mathbf{e} = (1, 1, \dots, 1)^T$ .

It was assumed by Anissimov *et al.* (1997) that the coefficients of exchange  $k_{ij}$  are typically proportional to the average number of mixing sites  $N_{mix}$  along the sinusoids. More precisely, for each  $i$ ,

$$T \max_{j \neq i} (k_{ij}) = \alpha N_{mix}, \quad (11)$$

where  $T$  is the average time of passage through the liver, and  $\alpha$  is the coefficient of proportionality of order 1. If it is further assumed that  $N_{max} \gg 1$  and therefore  $T \max_{j \neq i} m_{ij} \gg 1$ , then the solution of eqn (8) can be represented by the asymptotic series

$$\begin{aligned} \mathbf{c}(x, t) = & \mathbf{e} k^{1/2} c_0(z, t) + \mathbf{c}^{(1)}(z, t) \\ & + k^{-1/2} \mathbf{c}^{(2)}(z, t) + \dots, \end{aligned} \quad (12)$$

where  $k \gg 1$  is such that  $k^{-1} T \max_{j \neq i} m_{ij} \sim 1$ ;  $c_j^{(i)}(z, t) = O(1)$  for  $z = (L/v_{av})O(1)$  and  $c_j^{(i)}(z, t) \rightarrow 0$  for  $|z| \gg T = L/v_{av}$  as  $k \rightarrow \infty$ , with

$$z = k^{1/2}(t - x/v_{av}), \quad (13)$$

and  $v_{av}$  the average sinusoidal velocity.

It was found in terms of the variables  $x$  and  $t$ , that the partial differential equation for  $c_0$  is equivalent to the equation for the convection–dispersion model of hepatic elimination (Roberts & Rowland, 1985):

$$\begin{aligned} \frac{\partial c_0(x, t)}{\partial t} = & -v_{av} \frac{\partial c_0(x, t)}{\partial x} \\ & + D \frac{\partial^2 c_0(x, t)}{\partial x^2} - k_{av} c_0(x, t). \end{aligned} \quad (14)$$

The dispersion coefficient  $D$  is defined here in terms of parameters of the interconnected-tubes model (Anissimov *et al.*, 1997) by

$$D = \frac{\mathbf{a}^T (\mathbf{V} - v_{av} \mathbf{I}) \mathbf{w}^{(1)}}{Ak} v_{av}, \quad (15)$$

where  $\mathbf{I}$  is a unit matrix and  $\mathbf{w}^{(1)}$  is the solution of the linear algebraic equations

$$\mathbf{R} \mathbf{w}^{(1)} = \mathbf{b} = \mathbf{e} - \frac{\mathbf{v}}{v_{av}}, \quad \mathbf{e}^T \cdot \mathbf{w}^{(1)} = 0, \quad (16)$$

and  $\mathbf{R} = k^{-1} \mathbf{M}$ , so that  $\max_{i \neq j} (r_{ij}) \sim v_{av}/L$ .

For the dimensionless dispersion number (Roberts & Rowland, 1986a), we then have

$$D_N = \frac{D}{Lv_{av}} = \frac{\mathbf{a}^T (\mathbf{V} - v_{av} \mathbf{I}) \mathbf{w}^{(1)}}{AkL}. \quad (17)$$

Although the heterogeneity of the elimination rates was modelled in eqn (8) by the term  $\mathbf{K}_e$ , its zeroth-order approximation (14) is independent of this heterogeneity. In particular, the dispersion number defined in eqn (17) is independent of the heterogeneity of the elimination rates and is determined only by the distribution of velocity, as defined by  $\mathbf{v}$ , and the strength and structure of interconnections as defined by  $\mathbf{w}^{(1)}$ . It is therefore reasonable to call  $D_N$  in eqn (17) the vascular

dispersion number  $D_N^V$ , as determined for example by the outflow concentration–time profile of a non-extracted vascular marker (Roberts *et al.*, 1990).

### 3. The Steady State

In the steady state, the time derivative approaches zero in eqn (8) and we have

$$\mathbf{V} \frac{d\mathbf{c}}{dx} = -\mathbf{K}_e \mathbf{c} + \mathbf{M} \mathbf{c}, \tag{18}$$

with the boundary condition

$$\mathbf{c}(0) = c_{in} \mathbf{e}, \tag{19}$$

where  $c_{in}$  is the input concentration of drug common to all sinusoids.

$$c_2 = c_{in} \exp\left(\frac{xd}{2v_1v_2}\right) \times \left[ \frac{d - 2v_1k_{e2}}{b} \sinh\left(\frac{xb}{2v_1v_2}\right) + \cosh\left(\frac{xb}{2v_1v_2}\right) \right], \tag{21}$$

where

$$b = \sqrt{(v_2(m + k_{e1}) - v_1(\gamma m + k_{e2}))^2 + 4\gamma k^2 v_1 v_2}$$

and

$$d = v_2(m + k_{e1}) + v_1(\gamma m + k_{e2}).$$

For the case of strong interconnection between tubes ( $m = kr$ , with  $k \gg 1$  and  $r \sim v_{av}/L$ ), one can easily obtain the first-order approximations to  $c_1$  and  $c_2$  for large  $k$ :

$$\begin{aligned} c_1(x) &= c_{in} \exp\left(-\frac{k_{av}}{v_{av}}x\right) \left[ 1 + \frac{1}{k} \frac{(k_{e2}v_1 - k_{e1}v_2)[x\gamma(k_{e2}v_1 - k_{e1}v_2) + v_2(\gamma v_1 + v_2)]}{r(\gamma v_1 + v_2)^3} \right], \\ c_2(x) &= c_{in} \exp\left(-\frac{k_{av}}{v_{av}}x\right) \left[ 1 + \frac{1}{k} \frac{(k_{e1}v_2 - k_{e2}v_1)[x\gamma(k_{e1}v_2 - k_{e2}v_1) + v_1\gamma(\gamma v_1 + v_2)]}{r(\gamma v_1 + v_2)^3} \right], \end{aligned} \tag{22}$$

For two tubes ( $n = 2$ ), eqn (18) is a pair of coupled linear first-order differential equations. Taking into account properties (10), the matrix  $\mathbf{M}$  can be written as

$$\mathbf{M} = m \begin{pmatrix} -1 & 1 \\ \gamma & -\gamma \end{pmatrix}, \tag{20}$$

where  $m = m_{12}$  and  $\gamma = a_1/a_2$ . The solution of eqn (18) with boundary condition (19) is, for  $n = 2$ ,

$$c_1 = c_{in} \exp\left(\frac{xd}{2v_1v_2}\right) \times \left[ \frac{d - 2v_2k_{e1}}{b} \sinh\left(\frac{xb}{2v_1v_2}\right) + \cosh\left(\frac{xb}{2v_1v_2}\right) \right],$$

We note that these asymptotic formulae are correct only if  $\exp(-krx(\gamma/v_2 + 1/v_1))$  can be neglected, that is for not very small values of  $x$ .

For the flow-weighted output concentration  $c_{out}$  we have

$$\begin{aligned} c_{out} &= \frac{a_1v_1c_1(L) + a_2v_2c_2(L)}{a_1v_1 + a_2v_2} \\ &= \frac{\gamma v_1c_1(L) + v_2c_2(L)}{\gamma v_1 + v_2}, \end{aligned}$$

and substituting  $c_1$  and  $c_2$  from eqn (22) we get

$$c_{out} = c_{in} \exp\left(-\frac{k_{av}}{v_{av}}L\right) \times \left[ 1 + \frac{1}{k} \frac{\gamma L(k_{e1}v_2 - k_{e2}v_1)^2}{(\gamma v_1 + v_2)^3} \right]. \tag{23}$$

The form of the asymptotic series expansion for large  $k$ , as follows from eqn (22), is

$$c_i = f_0(x) + k^{-1} f_i^{(1)}(x) + k^{-2} f_i^{(2)}(x) + \dots, \quad (24)$$

$$i = 1, 2,$$

where  $f_0$  and  $f_i^{(j)}$  are some functions of  $x$  which are  $O(1)$  as  $k \rightarrow \infty$ . Note that this form is different from eqn (12), the form obtained for bolus input.

Having the exact solution, and the approximation to it for large  $k$ , in the case of two tubes, we can now analyse the steady-state case for a system of  $n$  interconnected tubes. As in the time-dependent case, we consider  $m_{ij} = kr_{ij}$  with  $k \gg 1$ , so that  $\max_{i \neq j} (r_{ij}) \sim v_{av}/L$ . Given the form of approximation (24) for large  $k$  in the case of two tubes, it is reasonable to expect for  $\mathbf{c}$  an asymptotic series expansion of the form

$$\mathbf{c}(x) = \mathbf{e}c_0(x) + \frac{1}{k} \mathbf{c}^{(1)}(x) + \frac{1}{k^2} \mathbf{c}^{(2)}(x) + \dots, \quad (25)$$

which should not be valid for very small values of  $x$ . We will represent  $\mathbf{c}^{(i)}$  by two components, one parallel to and one orthogonal to  $\mathbf{e}$ ,

$$\mathbf{c}^{(i)}(x) = \mathbf{e}c_0^{(i)}(x) + \mathbf{d}^{(i)}(x), \quad (26)$$

and substitute eqn (25) into eqn (18), with  $\mathbf{M} = k\mathbf{R}$ . Grouping terms with the same power of  $k$  yields

$$k^0: \mathbf{v} \frac{d}{dx} c_0(x) = -\mathbf{k}_e c_0(x) + \mathbf{R} \mathbf{d}^{(1)}(x), \quad (27)$$

$$k^{-1}: \mathbf{v} \frac{d}{dx} c_0^{(1)}(x) + \mathbf{V} \frac{d}{dx} \mathbf{d}^{(1)}(x) = -\mathbf{k}_e c_0^{(1)}(x) - \mathbf{K}_e \mathbf{d}^{(1)}(x) + \mathbf{R} \mathbf{d}^{(2)}(x), \quad (28)$$

$$k^{-i}: \mathbf{v} \frac{d}{dx} c_0^{(i)}(x) + \mathbf{V} \frac{d}{dx} \mathbf{d}^{(i)}(x) = -\mathbf{k}_e c_0^{(i)}(x) - \mathbf{K}_e \mathbf{d}^{(i)}(x) + \mathbf{R} \mathbf{d}^{(i+1)}(x), \quad (29)$$

where  $i \geq 2$ ,  $\mathbf{v}^T = (\mathbf{V}\mathbf{e})^T = (v_1, v_2, \dots, v_n)$  and  $k_e^T = (\mathbf{K}_e \mathbf{e})^T = (k_{e1}, k_{e2}, \dots, k_{en})$ . We now multiply

eqn (27) by  $\mathbf{a}^T$  on the left, and using  $\mathbf{a}^T \mathbf{R} = 0$  we get

$$\frac{dc_0(x)}{dx} = -\frac{\mathbf{a}^T \mathbf{k}_e}{\mathbf{a}^T \mathbf{v}} c_0(x) = -\frac{k_{av}}{v_{av}} c_0(x), \quad (30)$$

as we have  $\mathbf{a}^T \mathbf{v} = Av_{av}$  and  $\mathbf{a}^T \mathbf{k}_e = Ak_{av}$ . Thus, the zeroth-order approximation for the steady-state leads to a single tube equation, or the tube model (Bass *et al.*, 1976), with the elimination rate  $k_{av}$  and the flow velocity  $v_{av}$ . The solution of eqn (30) is

$$c_0(x) = C_1 \exp\left(-\frac{k_{av}}{v_{av}} x\right), \quad (31)$$

where  $C_1$  is an arbitrary constant. To fix  $C_1$ , we cannot directly use the boundary condition (19), as the asymptotic expansion (25) and thus the differential equation (30) for  $c_0(x)$  is not valid for very small  $x$ . Instead, we will later use a comparison with the two-tubes case to determine  $C_1$ .

Having substituted  $c_0(x)$  from eqn (31) into eqn (27), we get

$$\mathbf{R} \mathbf{d}^{(1)}(x) = k_{av} \left( \frac{\mathbf{k}_e}{k_{av}} - \frac{\mathbf{v}}{v_{av}} \right) c_0(x) \quad (32)$$

or

$$\mathbf{d}^{(1)}(x) = k_{av} \mathbf{u}^{(1)} c_0(x), \quad (33)$$

where  $\mathbf{u}^{(1)}$  is the solution of the linear algebraic equations

$$\mathbf{R} \mathbf{u}^{(1)} = \left( \frac{\mathbf{k}_e}{k_{av}} - \frac{\mathbf{v}}{v_{av}} \right), \quad \mathbf{e}^T \mathbf{u}^{(1)} = 0. \quad (34)$$

The solution of eqn (34) exists and is unique because  $\mathbf{R}$  shares the property (10) with  $\mathbf{M}$ .

We note that in the case of uniform elimination rates, where  $\mathbf{k}_e = k_{av} \mathbf{e}$ , eqn (34) can be written as

$$\mathbf{R} \mathbf{u}^{(1)} = \left( \mathbf{e} - \frac{\mathbf{v}}{v_{av}} \right), \quad \mathbf{e}^T \mathbf{u}^{(1)} = 0. \quad (35)$$

Comparing this equation with the definition of  $\mathbf{w}^{(1)}$  in eqn (16), it is easily seen that

$$\mathbf{u}^{(1)} = \mathbf{w}^{(1)}. \quad (36)$$

To find  $c_0^{(1)}(x)$ , we multiply eqn (28) by  $\mathbf{a}^T$  from the left, use  $\mathbf{a}^T \mathbf{R} = 0$  again, and substitute  $\mathbf{d}^{(1)}(x)$  in the form (33). The equation for  $c_0^{(1)}(x)$  is now

$$\begin{aligned} Av_{av} \frac{dc_0^{(1)}(x)}{dx} + Ak_{av}c_0^{(1)}(x) \\ = k_{av} \left( \mathbf{a}^T \mathbf{V} \mathbf{u}^{(1)} \frac{k_{av}}{v_{av}} - \mathbf{a}^T \mathbf{K}_e \mathbf{u}^{(1)} \right) c_0(x). \end{aligned} \quad (37)$$

The general solution of this differential equation is

$$c_0^{(1)}(x) = C_1(C_2 + Bx) \exp\left(-\frac{k_{av}}{v_{av}}x\right), \quad (38)$$

where

$$B = \frac{k_{av}^2}{Av_{av}^2} \mathbf{a}^T \left( \mathbf{V} - v_{av} \frac{\mathbf{K}_e}{k_{av}} \right) \mathbf{u}^{(1)}, \quad (39)$$

and  $C_2$  is another constant.

Thus, the first-order approximation is

$$\begin{aligned} \mathbf{c}(x) = C_1 \exp\left(-\frac{k_{av}}{v_{av}}x\right) \\ \times \left( \mathbf{e} + \frac{k_{av}}{k} \mathbf{u}^{(1)} + \frac{1}{k} \mathbf{e} (C_2 + Bx) \right). \end{aligned} \quad (40)$$

The corresponding approximation to the flow-weighted output concentration is

$$\begin{aligned} c_{out} &= \frac{\mathbf{a}^T \mathbf{V} \mathbf{c}(L)}{\mathbf{a}^T \mathbf{v}} \\ &= C_1 \exp\left(-\frac{k_{av}}{v_{av}}L\right) \left( 1 + \frac{1}{k} BL \right. \\ &\quad \left. + \frac{1}{k} \left( C_2 + \frac{k_{av} \mathbf{a}^T \mathbf{V} \mathbf{u}^{(1)}}{\mathbf{a}^T \mathbf{v}} \right) \right). \end{aligned} \quad (41)$$

To find the constants  $C_1$  and  $C_2$  we may use a comparison with the two-tubes case. Comparing eqn (23) with eqn (41) we see that  $C_1 = c_{in}$ . In eqn (23), the term of order  $k^{-1}$  is proportional

to  $L$ , so that in eqn (41) the third term in parentheses must be zero, that is

$$C_2 = -\frac{k_{av} \mathbf{a}^T \mathbf{V} \mathbf{u}^{(1)}}{\mathbf{a}^T \mathbf{v}}, \quad (42)$$

and for the output concentration we have

$$c_{out} = c_{in} (1 + H_N R_N^2) e^{-R_N}, \quad (43)$$

where

$$H_N = \frac{\mathbf{a}^T (\mathbf{V} - v_{av} \mathbf{K}_e / k_{av}) \mathbf{u}^{(1)}}{AkL}, \quad (44)$$

which we call the heterogeneity number, and  $R_N$  is the efficiency number eqn (2). It is clear from definition (44) that  $H_N$  takes into account not only heterogeneity of flow rates, as described by  $D_N^V$ , but variations of enzyme activity as well.

When elimination rates in all tubes are the same, then  $\mathbf{u}^{(1)} = \mathbf{w}^{(1)}$  as in eqn (36), and  $\mathbf{K}_e / k_{av} = \mathbf{I}$ . Hence, defining  $D_N^V$  by eqn (17), and  $H_N$  by eqn (44), it is evident that  $H_N = D_N^V$  in this case. It is obvious from eqn (44) that for the case of full correlation between  $\{k_{ej}\}$  and  $\{v_j\}$ , that is  $(k_{ej} - k_{av})/k_{av} = (v_j - v_{av})/v_{av}$ , we have  $H_N = 0$  and therefore  $H_N < D_N^V$ . For full anti-correlation (also called full inverse correlation or full negative correlation), when  $(k_{ej} - k_{av})/k_{av} = -(v_j - v_{av})/v_{av}$  (for positiveness of  $\{k_{ej}\}$  and  $\{v_j\}$  in this case we need to limit distributions so that  $\max k_{ei} \leq 2k_{av}$  and  $\max v_i \leq 2v_{av}$ ) comparison of eqns (44) and (17) gives instead  $H_N = 4D_N^V$  and therefore  $H_N > D_N^V$ . This analysis gives some idea as to what the dependence of  $H_N$  on relative distribution of velocities and elimination rates could be for an arbitrary system of interconnected tubes.

We note that the heterogeneity of enzyme distribution described by Bass *et al.* (1987) [the term  $\bar{\rho}^2 / \bar{\rho}^2$  in eqn (6)] is due to the distribution of enzyme along sinusoids and is different from the heterogeneity of elimination rates considered in this paper, which is due to the different enzyme activities in different sinusoids (transverse distribution of enzyme). In fact, because we assumed, for simplicity, that each  $k_{ei}$  is constant along the

corresponding tube, it follows that  $\rho$  is independent of  $x$  in our analysis, and hence  $\overline{\rho^2}/\bar{\rho}^2 = 1$  in eqn (6).

**4. The Dispersion and Heterogeneity Numbers**

Equations (17) and (44) give a quantitative definition for the dispersion and heterogeneity numbers, previously described only qualitatively by Roberts & Rowland (1986a). Unfortunately, these equations involve vectors  $\mathbf{w}^{(1)}$  and  $\mathbf{u}^{(1)}$  which are solutions to linear algebraic equations (16) and (34), and cannot be expressed in a simple form for a general system of interconnected tubes. In order to throw some light on these expressions, we will consider a few specific examples where the expressions for the vectors  $\mathbf{w}^{(1)}$  and  $\mathbf{u}^{(1)}$ , and thus for  $D_N^V$  and  $H_N$ , are simple.

As a simple example of a model  $n$ -tube system, we consider first the case of  $n$  tubes with equal cross-sectional areas ( $a_i = A/n$ ) and interconnections between neighbouring tubes, so that each tube is connected to two tubes, except the first and last which are connected to only one neighbouring tube. We will consider equal rates of exchange between tubes. The coefficient of interconnections in this case is

$$k_{ij} = kr(\delta_{ij-1} + \delta_{i-1j}), \quad i \neq j,$$

and the matrix  $\mathbf{R}$  is

$$\mathbf{R} = r \begin{pmatrix} -1 & 1 & 0 & \dots & & 0 \\ 1 & -2 & 1 & 0 & \dots & 0 \\ 0 & 1 & -2 & 1 & 0 & \dots & 0 \\ \vdots & & & & & & \vdots \\ 0 & \dots & & 0 & 1 & -1 \end{pmatrix}$$

Using this matrix to solve eqns (34) yields for  $\mathbf{u}^{(1)}$ :

$$u_i^{(1)} = \frac{1}{r} \left( \sum_{j=1}^{i-1} (i-j)b_j - \frac{1}{n} \sum_{k=2}^n \sum_{j=1}^{k-1} (k-j)b_j \right), \tag{45}$$

where  $b_i = k_{ei}/k_{av} - v_i/v_{av}$ .

As all tubes have equal cross-sectional areas, then  $\mathbf{a}^T = A\mathbf{e}^T/n$ , and

$$\mathbf{a}^T(\mathbf{V} - v_{av}\mathbf{K}_e/k_{av}) = \frac{A}{n}(\mathbf{v}^T - \mathbf{k}_e^T v_{av}/k_{av}) = \frac{Av_{av}}{n} \mathbf{b}^T,$$

so that formula (44) for  $H_N$  simplifies to

$$H_N = \frac{v_{av}}{nkL} \mathbf{b}^T \mathbf{u}. \tag{46}$$

Using eqn (45) for  $\mathbf{u}^{(1)}$  and taking into account that  $\mathbf{b}^T \mathbf{e} = 0$ , we get

$$H_N = -\frac{v_{av}}{nkrL} \sum_{i=2}^n \sum_{j=1}^{i-1} (i-j)b_j b_i.$$

This equation can be rewritten as

$$H_N = \frac{1}{nkrLv_{av}k_{av}^2} \sum_{i=2}^n \left( \sum_{j=1}^{i-1} (k_{ej}v_{av} - v_jk_{av}) \right)^2. \tag{47}$$

To get an expression for  $D_N^V$ , we simply need to take  $\mathbf{k}_e/k_{av} = \mathbf{e}$  (as for the uniform elimination rates  $D_N^V = H_N$ ) in eqn (47), thus

$$D_N^V = \frac{1}{nkrLv_{av}} \sum_{i=2}^n \left( \sum_{j=1}^{i-1} (v_{av} - v_j) \right)^2. \tag{48}$$

It is easy to see now that  $D_N^V$  and  $H_N$  are positive for any  $n$  in this model system. Note as well that eqn (47) for  $H_N$  can be written in a form somewhat similar to that of  $\varepsilon^2$  in eqn (3). Indeed, as  $av_j = f_j$ ,  $av_{av} = F$  and  $krT = krL/v_{av} = \alpha N_{mix}$  as in eqn (11), then eqn (47) can be modified to

$$H_N = \frac{1}{F^2 \alpha N_{mix}} \sum_{i=2}^n \left( \sum_{j=1}^{i-1} f_j \left( \frac{k_{ej}/k_{av}}{v_j/v_{av}} - 1 \right) \right)^2.$$

Another model system which we can analyse consists of  $n$  tubes all connected to each other. Cross-sectional areas of tubes and rates of exchange between tubes are again assumed equal.

Coefficients of exchange will be  $k_{ij} = kr, i \neq j$ , and in this case the matrix  $\mathbf{R}$  is

$$\mathbf{R} = \begin{pmatrix} -(n-1) & 1 & \cdots & 1 \\ 1 & -(n-1) & 1 & \cdots & 1 \\ \vdots & & & & \vdots \\ 1 & \cdots & 1 & -(n-1) \end{pmatrix}.$$

Using this matrix we get for  $H_N$ ,

$$H_N = \frac{1}{n^2 k L v_{av} k_{av}^2} \sum_{i=1}^n (k_{ej} v_{av} - v_j k_{av})^2. \quad (49)$$

Taking  $k_e/k_{av} = e$  we get for  $D_N^V$

$$D_N^V = \frac{1}{n^2 k L v_{av}} \sum_{i=1}^n (v_{av} - v_j)^2. \quad (50)$$

Once again, these expressions for  $H_N$  and  $D_N^V$  are obviously positive.

Equations (47)–(50) show how  $H_N$  and  $D_N^V$  depend on the distribution of velocities and elimination rates for the two simple model systems of interconnected tubes considered in this section.

While it is not yet proved that  $H_N$  and  $D_N^V$  defined in eqns (44) and (17) are positive for any system of interconnected tubes, the two examples considered here give some ground to believe that this is true in general, as would be expected intuitively.

It is interesting to note that in terms of interconnections between tubes, the first model system considered in this section represents ‘minimal’ coupling and the second ‘maximal’ coupling. In the first case, each tube is connected only to neighbouring tubes, whereas in the second case all the tubes are connected with each other. Comparing expressions for the dispersion number for the first case, eqns (47) and (48), with expressions for the second case, eqns (49) and (50), one can see that the dispersion number for the maximal coupling is much less than for the minimal coupling. In fact,  $D_{N1}^V \geq n D_{N2}^V$ , where  $D_{N1}^V$  and  $D_{N2}^V$  are dispersion numbers for the first

and the second cases, respectively. Together with  $D_N^V$  being proportional to  $1/k$ , this leads to the conclusion that the heterogeneity of transit times through the liver decreases with increase of coupling between sinusoids. It is not clear, yet, to what degree this conclusion is due to the particular way of modelling of interconnections between the sinusoids in eqn (8). We hope to verify this dependence of the heterogeneity of transit times on the strength of coupling in future by directly modelling discrete systems of interconnected tubes on the computer.

It was shown previously (Anissimov *et al.*, 1997) that for two interconnected sinusoids, the coefficient of interconnection  $k_{12}$  can be approximated using

$$k_{12} T = k_{12} L / v_{av} \approx \alpha N, \quad (51)$$

where  $\alpha \approx 0.7$  and  $N$  is the number of interconnections between two sinusoids. Extending eqn (51) to a system of  $n$  interconnected tubes we have

$$k_{ij} T \approx \alpha N_{ij}, \quad (52)$$

where  $N_{ij}$  is the number of interconnections between the  $i$ -th and  $j$ -th sinusoids. Summation of eqn (52) with respect to index  $j$  and then averaging for an entire system of  $n$  tubes yields

$$\overline{\sum_{j \neq i} k_{ij} T} \approx \alpha N_{mix}, \quad (53)$$

where  $N_{mix}$  is the average number of sinusoids connected to any one sinusoid. Applying eqn (53) to the model systems considered in this section it is possible to approximate  $krT$ :

$$krT \approx \alpha N_{mix} \frac{n}{2(n-1)} \quad (54)$$

for the model system with ‘minimal’ coupling, and

$$krT \approx \alpha N_{mix} \frac{1}{n-1} \quad (55)$$

for the model system with ‘maximal’ coupling.

Using eqns (54) and (55), eqns (48) and (50) can be written for the two-model systems as

$$D_{N1}^V \approx \frac{1}{\alpha N_{mix}} \frac{2(n-1)}{n^2} \sum_{i=2}^n \left( \sum_{j=1}^{i-1} \left( 1 - \frac{v_j}{v_{av}} \right) \right)^2, \quad (56)$$

$$D_{N2}^V \approx \frac{1}{\alpha N_{mix}} \frac{n-1}{n^2} \sum_{i=1}^n \left( 1 - \frac{v_j}{v_{av}} \right)^2. \quad (57)$$

These formulae give some insight into the way in which the distribution of velocities, and the nature of interconnections, contribute to the dispersion number. It is possible to approximate  $D_N^V$  now if the distribution of  $v_j$  values and the average number of interconnections per sinusoid  $N_{mix}$  are known. We note though, that due to the simplified way of modelling interconnections in the model systems presented here, the number  $n$  in eqns (56) and (57) should not be regarded strictly as the number of sinusoids in the entire liver. It may be interpreted rather as the number of sinusoids which are strongly interconnected with each other.

The actual distribution of the velocity of flow in sinusoids is shown in Fig. 1; it was obtained from the data of Koo *et al.* (1975). The frequency distributions of the direct, interconnected and branching sinusoids were summed to get the frequency distribution for all sinusoids. Grouping all sinusoids into  $n$  sets with similar velocities and equal numbers of sinusoids in each set, we find  $v_j$ , with  $j = 1, \dots, n$ , as an average velocity of the  $j$ -th set. Using these  $v_j$  in eqns (56) and (57), together with  $\alpha = 0.7$  and  $N_{mix} = 5$  (Bass *et al.*, 1987), yields for  $D_N^V$ :

$n$	2	3	5	10	100
$D_{N1}^V$	0.0294	0.1001	0.3450	1.5727	173.56
$D_{N2}^V$	0.0294	0.0514	0.0712	0.0882	0.1138

where  $D_{N1}^V$  and  $D_{N2}^V$  are dispersion numbers for model systems with “minimal” and “maximal” couplings, respectively. It is interesting that the dispersion number is typically greater for “minimal” than “maximal” coupling. For  $n = 5$ , the values  $D_{N1}^V = 0.3450$  and  $D_{N2}^V = 0.0712$  provide

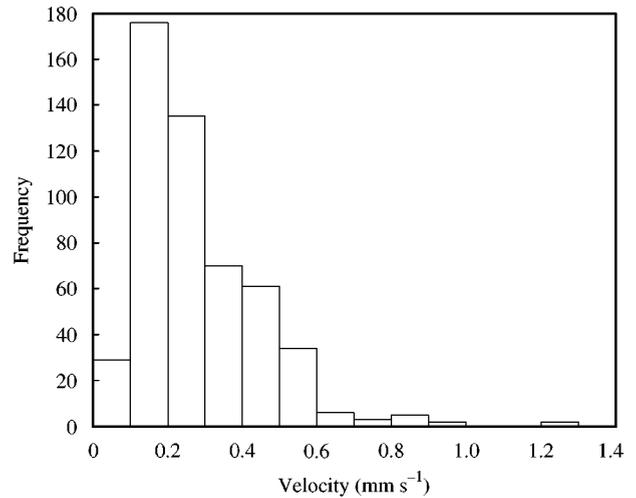


FIG. 1. Frequency distribution of the velocity of flow in sinusoids (adapted from Koo *et al.*, 1975).

reasonable upper and lower bounds, respectively, for experimental values of the dispersion number (Roberts *et al.*, 1988). The large values of  $D_{N1}^V$  for the model system with “minimal” coupling and with  $n \geq 10$ , are unrealistic, and probably arise because  $k$  is not big enough to validate the analysis in those cases. We recall that eqns (56) and (57) are only valid for  $k \geq 1$ ; in fact  $k$  is only about 3 for  $N_{mix} = 5$ .

It should be noted that the analysis of the value of the dispersion number presented here is very approximate. Further, using simplified model systems, we have not taken into account the heterogeneity of lengths of liver sinusoids. This heterogeneity might increase the effective heterogeneity of velocities, thus increasing the value of  $D_N^V$ .

## 5. Discussion

Further analyses of the interconnected-tubes model has been presented in this work. The approximation to the interconnected-tubes model for a large number of mixing sites ( $N_{mix} \gg 1$ ) for the steady-state input has been developed and results compared with that of bolus input.

It is interesting to compare the first-order approximation to the interconnected-tubes model, given by eqn (43), with the result for the dispersion model, where  $D_N$  for consistency must be

taken as a small parameter ( $D_N \ll 1$ ), because we have  $D = O(k^{-1})$ . Recognizing that  $c_{out} = c_{in}(1 - E)$ , and keeping only terms to the order of  $D_N$  in the approximation  $D_N \ll 1$  of the dispersion model (5), yields

$$c_{out} \approx c_{in}(1 + D_N^E R_N^2) e^{-R_N}, \quad (58)$$

where  $D_N^E$  is the dispersion number for extracted solutes in the steady state, as defined in eqn (6). This prediction of the dispersion model is equivalent to that of the interconnected-tubes model, as in eqn (43) with  $H_N = D_N^E$ . In the case of arbitrary elimination rates,  $H_N \neq D_N^V$ , and therefore  $D_N^V \neq D_N^E$ . We see that, because of its approximate nature, the dispersion model equation (14) cannot be applied to the steady state and bolus input cases with the same dispersion number, when substantial enzyme heterogeneity exists.

Owing to the inclusion of the intermixing terms in equations for the interconnected-tubes model,  $H_N$  depends now not only on distributions of  $k_{ei}$  and  $v_i$ , as does  $\varepsilon^2$ , but also on the extent and the structure of the intermixing between the sinusoids. In eqn (44), the parameters  $k$  and  $\mathbf{u}^{(1)}$  (which itself depends on  $\mathbf{R}$ ) determine this dependence of  $H_N$  on intermixing.

An important theoretical result for the distributed model is its prediction that  $\varepsilon^2$  is independent of small changes in the hepatic blood flow  $F$ . We shall now examine whether  $H_N$  depends on  $F$ . Suppose that a change of  $F$  is small enough not to change the shape of the distribution of velocities  $v_i$  in sinusoids; more precisely, suppose that  $v_i \propto F$  for all  $i$ . Then, for the average velocity (4) we also have  $v_{av} \propto F$ . It was argued already in eqn (11) that  $T \max_{j \neq i} k_{ij} = \alpha N_{mix}$ , and with  $N_{mix}$  unchanged and  $T = L/v_{av} \propto 1/F$ , we have for the coefficient of exchange,  $k_{ij} \propto F$ . Then  $r_{ij} \propto F$ , as we expect  $k$  to be flow-independent. Using eqn (34), we now obtain  $\mathbf{u}^{(1)} \propto 1/F$ . Finally, using eqn (44) it is easy to see that  $H_N$  is independent of small changes of the hepatic blood flow. This result is in agreement with the experimental data for the steady state (Bass, 1980). Similar analysis for the vascular dispersion number shows that  $D_N^V$  is also independent of small changes of the hepatic blood flow, in agreement with experiments (Roberts *et al.*, 1990a).

The zeroth-order approximation to the interconnected-tubes model for bolus input results in the convection–dispersion–reaction equation (14) (Anissimov *et al.*, 1997). In contrast, for the steady state, the zeroth-order approximation gives the convection equation (30). The understanding of this apparently contradictory result comes with the analysis of the order of magnitude of each term in eqns (8) and (18). In eqn (8), the derivatives  $\partial \mathbf{c} / \partial x$  and  $\partial \mathbf{c} / \partial t$  are of a higher order in the expansion parameter of  $k$  than is  $\mathbf{c}$ , because  $\mathbf{c}(x, t)$  is sharply peaked at  $x = tv_{av}$ . However in eqn (18),  $d\mathbf{c}/dx$  is of the same order of magnitude as  $\mathbf{c}$ . As  $D = O(k^{-1})$  according to eqn (15), so  $D_N^V \ll 1$ , and the term  $Dd^2c_0/dx^2$  disappears in the zeroth-order approximation of eqn (14) as a steady-state expression. Hence, eqn (14) is equivalent to eqn (30) in the steady-state case.

The comparison of the steady-state case and the case of bolus input leads to the realisation that the dispersion model, when viewed as an approximation to the interconnected-tubes model, does not comply with familiar notions of linear modelling when enzyme heterogeneity exists. We would normally expect that the response of the system to the unit impulse input (Green's function) defines the response for any input. However, eqn (43), the approximation to the interconnected-tubes model for the steady-state input, is not the same as the corresponding equation (58) for the dispersion model when  $H_N \neq D_N^V$ . The mathematical reason for this discrepancy being the approximate nature of the dispersion model when viewed as a limiting case of the interconnected-tubes model. This inability to use the Green's function for the dispersion model will be particularly troublesome if the input is an arbitrary function of time and if enzyme heterogeneity exists. We emphasize that when there is no distribution of elimination rates ( $\mathbf{k}_e = e\mathbf{k}_e$ ) over sinusoids, or its distribution is far narrower than the distribution of transit times (which could be the case for many drugs), the discrepancy between  $H_N$  and  $D_N^V$  disappears, and this difficulty along with it.

It should be emphasized that the present comparison of the interconnected-tubes model with the dispersion model is limited to the specific case where  $D_N^E \ll 1$ . The extent to which the results can be applied to hepatic elimination is uncertain

since physiologically observed  $D_N^V$  values range from 0.2 to 0.4.

Just as the Goresky and convection–dispersion models have two-compartment extensions (Goresky *et al.*, 1973; Roberts *et al.*, 1988; Yano *et al.*, 1989), so also the interconnected-tubes model could be extended by assuming two compartments within each tube: one cellular, with no longitudinal flow through it, and one vascular, with convective (longitudinal) transport. Exchange of drug between vascular and cellular compartments could be modelled with rates  $k_{1i}$  and  $k_{2i}$ , and elimination from cellular compartments with rates  $k_{eci}$ . The vascular volume of distribution, as defined by the tube cross-section  $a_i$ , is known to be dependent on the size of the “substance” being examined. Thus, erythrocytes are restricted to the sinusoidal space while albumin has a lower vascular volume of distribution than the smaller sucrose and sodium (Goresky, 1963). Distribution volumes which extend into the cellular compartments are often defined by the physiological distribution space for the unbound solute together with the relative binding in the vascular and cellular spaces (Weiss & Roberts, 1996). Such refinements to the interconnected-tubes model can be expected to yield similar outcomes, in terms of transit times and outflow concentration–time profiles, that predicted by the Goresky and convection–dispersion models.

Analysis of an interconnected-tubes model which includes heterogeneity of enzyme distribution in a two-compartment representation is considered to be possible but requires more complex mathematics. Other extensions can also be envisaged. Intrahepatic shunting, caused by cirrhosis for example, can also be modelled by assuming that a subset of affected sinusoids have elimination rates much lower than those of unaffected sinusoids. One implication of such a model of shunting will be larger heterogeneity of elimination rates, and therefore a larger discrepancy between  $D_N^V$  and  $H_N$ . In this work, the analysis of the interconnected-tubes model has been limited to a simple case where both elimination rates  $k_{ei}$ , and coefficients of exchange  $k_{ij}$ , are constant along tubes. These assumptions were made to allow some progress with the mathematics. For a numerical treatment of the model, these sim-

plifying assumptions can be relaxed, and more complex phenomena analysed. For example, it is then possible to model localised “zones” of elimination in the liver, allowing preferential elimination or metabolism in, say, the periportal zone of the liver acinus (Gumucio & Miller, 1981). It is only necessary to allow  $k_{ei}(x)$  to become functions which decrease with increasing  $x$ , perhaps in discrete steps. It has been argued that there are more interconnections between the sinusoids in the periportal region as compared to the previous region of acini (Gumucio, 1983). This structure of liver acini can also be modelled, by allowing the  $k_{ij}(x)$  to decrease as  $x$  increases.

Finally, we want to emphasize that mathematically, the convection–dispersion and distributed models can both be regarded as the limiting cases of the interconnected-tubes model. If there are few interconnections between tubes (that is  $k \approx 0$ ), then eqn (8) is essentially identical to the defining equations of the distributed model, whereas for  $k \gg 1$ , the zeroth-order approximation to eqn (8) is the defining partial differential equation of the convection–dispersion model, as we have shown. This ensures that the interconnected-tubes model can be made consistent with a wide range of experimental situations already successfully described using either the convection–dispersion or distributed models (Luxon & Weisiger, 1993; Rivory *et al.*, 1992; Roberts *et al.*, 1990a, b; Yano *et al.*, 1989; Bass *et al.*, 1987). It is an important challenge to devise new experiments which can discriminate among various models more effectively and in particular provide experimental checks of the more detailed interconnected-tubes model, and estimates of its parameters.

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